
AC 2012-3670: ENGINEERING FUTURE CHEMICAL ENGINEERS: INCORPORATION OF PROCESS INTENSIFICATION CONCEPTS INTO THE UNDERGRADUATE CURRICULUM

Dr. Rebecca K. Toghiani, Mississippi State University

Dr. Adrienne Robyn Minerick, Michigan Technological University

Adrienne Minerick is an Associate Professor of chemical engineering at Michigan Tech having moved from Mississippi State University in Jan. 2010, where she was a tenured Associate Professor. She received her M.S. and Ph.D. from the University of Notre Dame in 2003 and B.S. from Michigan Technological University in 1998. Minerick's research interests include electrokinetics and the development of biomedical microdevices. She earned a 2007 NSF CAREER Award and the 2011 Ray Fahien Award. Her group has published in the proceedings of the National Academy of Science, Lab on a Chip, and had an AIChE Journal cover. She is an active mentor of undergraduate researchers and served as co-PI on an NSF REU site. Research within her Medical micro-Device Engineering Research Laboratory (M.D. ERL) also inspires the development of Desktop Experiment Modules (DEMOS) for use in chemical engineering classrooms or as outreach activities in area schools. Adrienne has been an active member of ASEE's WIED, ChED, and NEE leadership teams since 2003.

Dr. Keisha B. Walters, Mississippi State University

Keisha B. Walters joined the chemical engineering faculty at Mississippi State University (MSU) in 2005, where she currently holds the rank of Associate Professor. A graduate of Clemson University, she received the Thomas Evans Instructional Paper Award (2009) and Best Paper Award (2010) from ASEE-SE. In 2010, she was inducted into MSU's Bagley College of Engineering Academy of Distinguished Teachers and also selected to participate in the National Academy of Engineering Frontiers of Engineering Education (FOEE) Symposium. Walters has been a member of ASEE since 2002. Her research interests focus on polymeric and biobased materials, nanotechnology, and surface and interface engineering.

Dr. Priscilla J. Hill, Mississippi State University

Priscilla Hill is currently an Associate Professor in the Dave C. Swalm School of Chemical Engineering at Mississippi State University. She has research interests in crystallization, particle technology, population balance modeling, and process synthesis. Her teaching interests include particle technology and thermodynamics.

Dr. Carlen Henington, Mississippi State University

Carlen Henington is a nationally certified School Psychologist and is an Associate Professor in school psychology at Mississippi State University. She completed her doctoral work at Texas A&M University and her internship at the Monroe Meyer Institute for Genetics and Rehabilitation at the University of Nebraska Medical Center, Omaha. She received the Texas A&M Educational Psychology Distinguished Dissertation Award in 1997, the Mississippi State University Golden Key National Honor Society Outstanding Faculty Member Award in 2000, the Mississippi State University Phi Delta Kappa Outstanding Teaching Award in 1998, and the College of Education Service Award in 2010. She has worked as a consultant to the Mississippi Department of Education to address disproportionality and has provided technical assistance to schools across the state. She has served as a program reviewer for the American Psychological Association and for the National Association for School Psychologists for more than eight years. Additional areas of research include evaluation of effective teaching and program administration at the post-secondary levels.

**Engineering Future Chemical Engineers: Incorporation of
Process Intensification Concepts into the Undergraduate
Curriculum: Year 3 Activities**

Abstract

Year 3 activities focused on incorporating concepts of process intensification into four chemical engineering courses are presented. These activities provide undergraduate chemical engineers with an introduction to process intensification, and the opportunity to learn about key aspects of combining processes/operations to achieve enhancements in energy efficiency, improved safety, utilization of resources and reduction of capital costs, waste generation, and energy consumption. Process intensification involves thinking about chemical processing in new ways such that (1) recognition of inherent limitations imposed by using sequential unit operations to accomplish chemical and/or physical transformations is achieved; and (2) methods of concurrently performing more than one unit operation are considered. This requires undergraduates to think in different ways about the processes they have learned about in their traditional unit operations courses. Process intensification is essential to industrial competitiveness as it can enhance safety, increase operating efficiency, lower energy usage, reduce capital costs, reduce waste emissions and process hazards, or encompass several of these benefits. Improving processes by process intensification requires engineers to integrate many fundamental concepts and go beyond traditional unit operations. Through activities focused on process intensification, global learning and the ability of our students to synthesize knowledge from different courses are strengthened.

Four core chemical engineering courses are targeted: fluid flow operations; heat transfer operations; mass transfer operations; and chemical reactor design. Over the course of this curriculum improvement project, activities/modules have been developed and incorporated into each course. Each activity/module focuses on a particular element from the process intensification spectrum and these are also designed to enhance vertical concept integration. Assessment data collected from the implementation of activities during Years 1 and 2 will also be presented.

Project Activities - Year 3

Kick Off Activity

At the start of the fall semester, Dr. Kishori Deshpande, Senior Research Engineer in Engineering Sciences at The Dow Chemical Company, visited the MSU campus and gave an invited presentation entitled "Achieving Sustainability through Process Intensification: An industrial perspective." During the seminar, Dr. Deshpande presented case studies of successful implementation of process intensification concepts at Dow. Approximately 75 students and faculty were in attendance at the seminar.

Fluid Flow Operations

The instructional module developed for year 3 for the fluids course will focus on the flow fields generated by centrifugal action. The traditional course content includes exposure to the use of a centrifugal field to separate two immiscible liquids that possess densities that differ only slightly from one another [1]. However, the use of the centrifugal field is presented only in the context of its effect on hydrostatic equilibrium. The use of centrifugal fields in chemical engineering to enhance processes through minimization of mass transfer resistance has applications in both

separations and in chemical reactors. As a prelude to examination of two key process intensification technologies, the HiGEE separator (mass transfer operations) and the spinning disk reactor (chemical reactor design), some exposure to the flow fields generated by centrifugal action is necessary. The introduction of the relevant coordinate system will be required. An overview of the development of the velocity profiles for each application will be provided, with specific activities examining influence of field strength and fluid properties on the fluid velocity profile. This activity will be conducted during the Fall 2012 semester.

Heat Transfer Operations

During year 3 in the Heat Transfer Operations course, instructional modules developed under the project will be used (3rd cycle for Heat Transfer Operations is the Spring 2012 semester). One module focuses on heat transfer in thin films and is designed to allow students to identify controlling phenomena with different terms in the energy balance. The module for year 3 will focus on a conceptual design of heat exchangers embodying the tenants of process intensification [2-4]. This activity will be completed during the Spring 2012 semester.

Mass Transfer Operations

During year 3 in the Mass Transfer Operations course, three instructional modules developed under the NSF-CCLI project will be used (the 3rd cycle for Mass Transfer Operations is the Spring 2012 semester). The first module examines the coupling of reaction and separation as implemented in reactive distillation. The instructional module presents the basic operation of a reactive distillation column and students complete a homework assignment examining an industrial application of the technology. The second module presents instruction regarding divided wall columns, and how this mode of construction/operation allows for increased energy efficiency. The third instructional module examines the concept of hybrid separation processes, where two distinct separation processes are coupled together, each operating in the regime where they offer superior performance. Review material for each of the individual separation processes is presented, along with basic process configuration. The advantages/disadvantages of each process are reviewed and limitations/constraints are also presented. Three case studies where hybrid separations have been successfully employed in industry are included in the module. These case studies examine the coupling of 1) pressure swing adsorption and membrane permeation for separation of nitrogen from natural gas; 2) distillation and vapor permeation or distillation and pervaporation for the separation of ethanol and water, and 3) distillation/facilitated transport for the separation of propane and propylene.

Chemical Reactor Design

During year 3, three instructional modules developed under the NSF-CCLI project were used in the Chemical Reactor Design course. The first module examined coupling of chemical reactions where either energy or mass or both energy and mass were exchanged to provide for increased energy and materials utilization efficiency. The second module examined the coupling of separation and reaction through the use of simulated moving bed reactor technology. The module provides background information on adsorption processes and how they work and are designed; the disadvantages of moving bed technology with regards to solids, and how simulated

moving bed technology overcomes these disadvantages. The coupling of the simulated moving bed separation technology with reaction is also examined with a case study of p-xylene production [5].

The third instructional module focuses on novel reactor configurations. For the production of fine chemicals and pharmaceuticals, chemical reactions are often carried out in batch rather than continuous mode. Two novel alternatives are the cavitation reactor [6] and the spinning disk reactor [7]. These utilize sonication and high gravity, respectively, to enhance mass transfer in the reactor, leading to significant performance improvements over batch reactors. The module provides instruction on the phenomena exploited to achieve the improvements in each reactor type and basic configuration as well as an overview of technology applications and commercial use. Reaction system yields/selectivity for the alternative reactors are compared to performance data for conventional reactors.

Assessment of Activities

Assessment results for Years 1-3 are discussed (see Table 1 for rotation of courses taught). Ratings of 269 students across 14 variables (Table 2-5) in all four classes (i.e., Mass Transfer Operations, Heat Transfer Operations, and Fluids Flow Operations, and Reactor Design) early in the semester (pre) and at the end of the semester (post) used a survey that consisted of ratings of 0 (Disagree), 1 (Somewhat Agree), 2 (Somewhat Agree), and 3 (Agree). Because this study is a multi-year study, students were enrolled in classes at various stages as they matriculated through the program of study for Chemical Engineering. Future studies will examine the students as they progressed through the program using single-subject design analyses. The current study examines only individual course results. Thus, Tables 2-5 provide the means at pre and post and the degree of change across rating times for each class during the semesters taught and as a total of all students enrolled in each class. For clarity, only ratings for all sections of a class (e.g., across all semesters) will be presented below.

At pre instruction, the ratings (depending upon variable) of a total of 52 to 57 students were matched across the two semesters in Heat Transfer (see Table 2). Students rated all 14 areas at higher levels at post instruction than at pre instruction with the exception of *Easily Presented* (Pre $M = 1.95$, $SD = 0.69$ and Post $M = 1.89$, $SD = 0.75$) showing that most students did not perceive the material to be easily presented by the instructor. However, only 6 of the 14 variable ratings were significantly higher at post instruction relative to pre instruction. These include: (a) *Used Activities to Illustrate*, $t(1,55) = (-4.69)$, $p = 0.000$; (b) *Furthered Understanding*, $t(1,54) = (-2.48)$, $p = 0.016$; (c) *Encouraged to Use Analysis*, $t(1, 51) = (-3.77)$, $p = 0.000$; (d) *Encouraged to Use Synthesis*, $t(1, 53) = (-2.84)$, $p = 0.042$; (e) *Can be Flexible*, $t(1, 56) = (-2.68)$, $p = 0.010$; and (f) *Can Integrate Outside Info*, $t(1, 55) = (-2.69)$, $p = 0.010$ (see Table 6).

In Mass Transfer, data could be matched (depending upon variable) for a total of 56 to 59 students across the two semesters. On average, all students provided lower post instruction than pre instruction ratings. Notably, the lowest ratings across both semesters were in *Used Activities to Illustrate* (post instruction $M = 1.30$, $SD = 0.93$), *Furthered Understanding* (post instruction $M = 1.77$, $SD = 1.02$), and *Encouraged to Use Synthesis* (post instruction $M = 1.98$, $SD = 0.87$). These ratings indicate students, on average Agreed Somewhat or less on these variables.

Relative to pre instruction, ratings at post instruction were not significantly different across both semesters for any of the variables with the exception of three: (a) *Used Activities to Illustrate*, $t(1, 56) = 2.08$, $p = 0.042$; (b) *Encouraged to Problem Solve*, $t(1, 58) = 2.08$, $p = 0.042$; and (c) *Can Use Analysis*, $t(1, 56) = 2.32$, $p = 0.024$ (see Table 7).

During the first semester the Fluid Flow Operations course was taught (Semester 3) with the intensification lecture component included, multiple student ratings were at or below Somewhat Agree (M range 1.51 to 2.28 on all 0 to 3 ratings and M range 4.07 to 4.40 on 0 to 6 ratings). Only two variables were significantly different pre to post instruction (both with lower ratings at post instruction): (a) *Easily Presented*, $t(1, 42) = 4.65$, $p = 0.000$ and (b) *Furthered Understanding*, $t(1, 42) = 2.96$, $p = 0.005$ (see Table 8). For this past semester (Semester 5) when the concept of process intensification was introduced, but with no subsequent module presentations, students rated only two variables lower (*Used Activities to Illustrate* and *Encouraged to Modify Materials/Knowledge*), neither was lower to a significant degree ($\Delta = (-0.08)$ and (-0.03) , respectively). However, seven of the variables were rated significantly higher, pre to post instruction, by students: (a) *Encouraged to be Flexible*, $t(1, 38) = (-2.40)$, $p < 0.021$; (b) *Encouraged to Problem Solve*, $t(1, 48) = (-2.40)$, $p < 0.021$; (c) *Encouraged to Integrate Outside Materials/Knowledge*, $t(1, 38) = (-2.93)$, $p < 0.006$; (d) *Encouraged to Use Analysis*, $t(1, 38) = (-5.23)$, $p < 0.000$; (e) *Encouraged to Use Synthesis*, $t(1, 38) = (-4.08)$, $p < 0.000$; (f) *Can be Flexible*, $t(1, 38) = (-2.70)$, $p < 0.010$; and (g) *Can Use Synthesis*, $t(1, 38) = (-3.14)$, $p < 0.003$ (see Table 9).

In Reactor Design (depending upon variable) a total 71 to 73 ratings could be paired across two semesters. On average across both semesters, relative to pre instruction, students rated all areas higher at post instruction, with five variables rated significantly higher on average. These variables included: (a) *Encouraged to be Flexible*, $t(1, 72) = (-2.08)$, $p < 0.041$; (b) *Encouraged to Problem Solve*, $t(1, 72) = (-2.08)$, $p < 0.041$; (c) *Encouraged to Integrate Outside Materials/Knowledge*, $t(1, 72) = (-2.00)$, $p < 0.049$; (d) *Encouraged to Use Analysis*, $t(1, 72) = (-2.48)$, $p < 0.016$; and (e) *Can Use Synthesis*, $t(1, 71) = -2.22$, $p < 0.030$ (see Table 10).

In the Reactor Design (both semesters) and Mass Transfer (one semester) courses, an integration activity was presented to students ($n=73$ and 36, respectively) and an evaluation of knowledge was administered pre and post activity. This activity consisted of 4 questions, 3 which possessed a single correct response and 1 that had multiple correct responses (select all that are correct). Thus, the maximum score possible was 6. The responses were grouped according to a single correct response on three questions (scored right or wrong; e.g., 3-question scores ranged from 0 to 3) and a multiple-choice question (scored 1 for each correct selection, e.g., 0 to 3). A paired sample t test was calculated to determine differences pre to post. In the Reactor Design course, students scored significantly better during post on the single response questions ($M = 2.68$, $SD = 0.72$) than during the pre activity ($M = 1.39$, $SD = 0.74$), $t(1, 92) = (-12.78)$, $p < 0.000$ and on the multiple response questions ($M = 1.41$, $SD = 0.91$ and $M = 2.82$, $SD = 0.47$, pre and post activity respectively), $t(1, 92) = (-15.10)$, $p < 0.000$. In the Mass Transfer course, students scored significantly better at post on the single response questions ($M = 2.61$, $SD = 0.77$) than at pre activity ($M = 1.28$, $SD = 0.66$), $t(1, 35) = (-8.94)$, $p < 0.000$ and on the multiple response questions ($M = 1.67$, $SD = 0.76$ and $M = 2.42$, $SD = 0.69$, pre and post activity respectively), $t(1,$

35) = (-5.84), $p < 0.000$. Results of the paired samples test are presented in Table 11 for both courses.

Integrity checks with class activities conducted two times during the semester in both courses indicated instructors were rated at relatively high levels across all variables (inter observer agreement at greater than 90% for all courses).

Summary/Discussion

Overall, students' perceptions are high across all 14 variables in all semesters that all four courses were taught (M range = 1.24-2.81 and 1.05-2.89, pre and post, respectively on a 0 to 3 point scale, 3=higher scores) and M range = 4.04-5.11 and 3.90-5.44, pre and post, respectively only a 0 to 6 point scale, 6=higher scores). There does appear to be a change in students' perceptions of the courses and their own abilities within specific classes, sometimes a positive change and sometimes a negative change. For students enrolled in Heat Transfer, the data show there is a gain in perception that the activities illustrate concepts and that the information is useful to further their understanding. However, these improved perceptions are not necessarily present in the perceptions of students in other courses. Additionally, students in Heat Transfer also appeared to perceive increases in three areas: encouragement to use analysis and synthesis; their ability to be flexible; and their ability to integrate outside information. Students enrolled in Reactor Design showed growth in encouragement to problem solve, to be flexible, to integrate outside materials/knowledge, and to use analysis. There was also an improvement of students' perception of their ability to synthesize information in Reactor Design.

There were a few situations where students' perceptions decreased within the class. Specifically, in Mass Transfer, students' perceptions of activities to illustrate concepts decreased as did perception of encouragement to problem solve and their ability to use analysis. In Fluid Flow, students' perceptions decreased in the usefulness of information to further their understanding.

Students in Mass Transfer and Reactor Design showed a growth in knowledge pre to post intensification instruction as indicated by significant change in their quiz scores.

It is important to recognize that because ratings were universally positive for all variables in all classes, a few lower ratings should not be a cause for concern. Nor is there yet sufficient information to determine specifics about the cause of decreased or increased perceptions. Further analyses will need to be conducted to examine relationships between student characteristics (e.g., course sequence, GPA) and teacher evaluations and classroom observations.

Conclusion

Integration of key concepts related to process intensification across multiple core chemical engineering courses provides the opportunity for students to become both familiar with the tenets of process intensification as well as be equipped to examine intensified process alternatives during the senior design courses. As students progress through the four-course sequence, it is expected that their foundation will become stronger in these tenets and they will be better

equipped to face the challenges that will be present when they graduate and enter the chemical engineering workforce.

Acknowledgement

This work was funded through the National Science Foundation under grant DUE-0837409.

References

- [1] McCabe, W.; Smith, J.; Harriott, P.; Unit Operations of Chemical Engineering, (7th edition, McGraw Hill, New York, NY (2004).
- [2] Ramshaw C.; "Comments on: Process intensification: heat and mass transfer characteristics of liquid films on rotating discs," A. Aoune and C. Ramshaw [*Intl. J. Heat & Mass Trans.* 42, 2543-2556 (1998)], *Intl. J. Heat & Mass Trans.* 43(15), 2822-2823, (2000).
- [3] Oxley, P.; Brechtelsbauer, C.; Ricard, F.; Lewis, N.; Ramshaw, C.; "Evaluation of Spinning Disk Reactor Technology for the Manufacture of Pharmaceuticals," *Ind. Eng. Chem. Res.* 39, 2175-2182 (2000).
- [4] Geraci G.; Azzopardi B.J.; van Maanen, H.R.E.; "Inclination effects on circumferential film flow distribution in annular gas/liquid flows," *AIChE J.*, 53(5), 1144-1150 (2007). AND Ramshaw C.; Cook S.; "Spinning Around," *TCE*, 774-5, 42-44, (2006).
- [5] UOP Honeywell, Schematic of Parex Process, 2006.
- [6] Gogate, P.R.; "Cavitation reactors for process intensification of chemical processing applications: A critical review," *Chemical Engineering and Processing*, 47, 515-527 (2008).
- [7] Oxley, P.; Brechtelsbauer, C.; Ricard, F.; Lewis, N.; Ramshaw, C.; "Evaluation of Spinning Disk Reactor Technology for the Manufacture of Pharmaceuticals," *Ind. Eng. Chem. Res.* 39, 2175-2182 (2000).

Table 1 Semesters Courses Were Taught and Number of Student Participants

Semester Taught	# Students
Heat Transfer	
Spring Semester 2	34
Spring Semester 4	23
Total	57
Mass Transfer	
Spring Semester 2	37
Spring Semester 4	21
Total	58
Fluid Flow	
Fall Semester 3	43
Fall Semester 5	39
Total	82
Reactor Design	
Fall Semester 3	37
Fall Semester 5	36
Total	73
Total Students	
Total Student Participants Across all Courses	269

Table 2 Change (Δ) Pre to Post in Students' Mean Perceptions Pre to Post in Heat Transfer Semester 2 ($n=34$), Semester 4 ($n=23$), and Total ($n=57$)

Variable	Semester 2			Semester 4			Total		
	Pre	Post	Δ	Pre	Post	Δ	Pre	Post	Δ
Easily Presented	1.88	1.88	0.00	2.04	1.91	-0.13	1.95	1.89	-0.06
Used Activities to Illustrate	1.24	2.56	1.32	2.18	1.91	-0.27	1.61	2.30	0.69
Furthered Understanding	1.58	2.52	0.94	2.18	1.77	-0.41	1.82	2.22	0.40
Encouraged to Modify Materials/Knowledge	2.32	2.35	0.03	2.13	2.26	0.13	2.25	2.32	0.07
Encouraged to be Flexible	2.35	2.53	0.18	2.30	2.50	0.20	2.33	2.52	0.19
Encouraged to Problem Solve	2.35	2.53	0.18	2.30	2.50	0.20	2.33	2.52	0.19
Encouraged to Integrate Outside Materials/ Knowledge	2.15	2.35	0.20	2.04	2.22	0.18	2.11	2.30	0.19
Encouraged to Use Analysis	4.17*	4.87*	0.70	4.14*	4.73*	0.59	4.15*	4.81*	0.66
Encouraged to Use Synthesis	2.06	2.41	0.35	2.27	2.45	0.18	2.15	2.43	0.28
Can be Flexible	1.97	2.35	0.38	2.04	2.26	0.22	2.00	2.32	0.32
Can Use Problem Solving	2.21	2.44	0.23	2.26	2.39	0.13	2.23	2.42	0.19
Can Integrate Outside Info	4.27*	4.67*	0.40	4.04*	4.61*	0.57	4.18*	4.64*	0.46
Can Use Analysis	1.94	2.30	0.36	2.26	2.30	0.04	2.07	2.30	0.23
Can Use Synthesis	2.13	2.32	0.19	2.09	2.35	0.26	2.11	2.33	0.22

Note: * indicates a rating scale of 0-6 (6=higher ratings), all other ratings on a scale of 0-4 (4=higher ratings), bold indicates significant ($p \leq 0.05$) difference.

Table 3 Change (Δ) Pre to Post in Students' Mean Perceptions Pre to Post in Mass Transfer Semester 2 ($n=37$), Semester 4 ($n=21$), and Total ($n=58$)

Variable	Semester 2			Semester 4			Total		
	Pre	Post	Δ	Pre	Post	Δ	Pre	Post	Δ
Easily Presented	2.49	2.32	-0.17	1.95	2.05	0.10	2.29	2.22	-0.07
Used Activities to Illustrate	1.67	1.44	-0.23	1.33	1.05	-0.28	1.54	1.30	-0.24
Furthered Understanding	2.06	1.92	-0.14	1.76	1.52	-0.24	1.95	1.77	-0.18
Encouraged to Modify Materials/ Knowledge	2.57	2.35	-0.22	2.23	2.36	0.13	2.44	2.36	-0.08
Encouraged to be Flexible	2.38	2.19	-0.19	2.18	1.95	-0.23	2.31	2.10	-0.21
Encouraged to Problem Solve	2.41	2.16	-0.25	2.18	1.95	-0.23	2.32	2.08	-0.24
Encouraged to Integrate Outside Materials/Knowledge	2.27	2.08	-0.19	1.86	2.14	0.28	2.12	2.10	-0.02
Encouraged to Use Analysis	4.06*	3.71*	-0.35	4.05*	3.90*	-0.15	4.05*	3.79*	-0.26
Encouraged to Use Synthesis	2.27	2.11	-0.16	1.90	1.76	-0.14	2.14	1.98	-0.16
Can be Flexible	2.33	2.39	0.06	2.09	2.18	0.09	2.24	2.31	0.07
Can Use Problem Solving	2.59	2.35	-0.24	1.91	2.18	0.27	2.34	2.29	-0.05
Can Integrate Outside Info	4.76*	4.43*	-0.33	4.36*	4.55*	0.19	4.61*	4.47*	-0.14
Can Use Analysis	2.51	2.06	-0.45	2.18	2.23	0.05	2.39	2.12	-0.27
Can Use Synthesis	2.35	2.35	0.00	2.05	2.18	0.13	2.24	2.29	0.05

Note: * indicates a rating scale of 0-6 (6=higher ratings), all other ratings on a scale of 0-4 (4=higher ratings), bold indicates significant ($p \leq 0.05$) difference.

Table 4 Change (Δ) Pre to Post in Students' Mean Perceptions Pre to Post in Fluid Flow Semester 3 ($n=43$) and Semester 5 ($n=39$)

Variable	Semester 3			Semester 5		
	Pre	Post	Δ	Pre	Post	Δ
Easily Presented	2.56	1.81	-0.75	2.21	2.50	0.29
Used Activities to Illustrate	1.70	1.60	-0.10	2.08	2.00	-0.08
Furthered Understanding	1.98	1.51	-0.47	2.13	2.37	0.24
Encouraged to Modify Materials/Knowledge	2.26	2.28	0.02	2.54	2.51	-0.03
Encouraged to be Flexible	2.19	2.26	0.07	2.31	2.62	0.31
Encouraged to Problem Solve	2.19	2.26	0.07	2.31	2.62	0.31
Encouraged to Integrate Outside Materials/Knowledge	2.47	2.33	-0.14	2.23	2.54	0.31
Encouraged to Use Analysis	4.42*	4.07*	-0.35	4.05*	4.95*	0.90
Encouraged to Use Synthesis	2.24	1.95	-0.29	1.82	2.54	0.72
Can be Flexible	2.09	1.91	-0.18	2.28	2.62	0.34
Can Use Problem Solving	2.26	2.21	-0.05	2.49	2.67	0.18
Can Integrate Outside Info	4.28*	4.40*	0.12	4.62*	4.97*	0.35
Can Use Analysis	2.13	1.90	-0.23	2.46	2.54	0.08
Can Use Synthesis	2.15	1.95	-0.20	2.18	2.51	0.33

Note: * indicates a rating scale of 0-6 (6=higher ratings), all other ratings on a scale of 0-4 (4=higher ratings), bold indicates significant ($p \leq 0.05$) difference.

Table 5 Change (Δ) Pre to Post in Students' Mean Perceptions Pre to Post in Reactor Design Semester 3 ($n=37$), Semester 5 ($n=36$), and Total ($n=73$)

Variable	Semester 3			Semester 5			Total		
	Pre	Post	Δ	Pre	Post	Δ	Pre	Post	Δ
Easily Presented	2.81	2.73	-0.08	2.67	2.89	0.22	2.74	2.81	0.07
Used Activities to Illustrate	2.11	1.90	-0.21	2.19	2.36	0.17	2.15	2.13	-0.02
Furthered Understanding	2.31	2.14	-0.17	2.40	2.63	0.23	2.35	2.38	0.03
Encouraged to Modify Materials/Knowledge	2.62	2.57	-0.05	2.47	2.75	0.28	2.55	2.66	0.11
Encouraged to be Flexible	2.62	2.76	0.14	2.61	2.83	0.22	2.62	2.79	0.17
Encouraged to Problem Solve	2.62	2.76	0.14	2.61	2.83	0.22	2.62	2.79	0.17
Encouraged to Integrate Materials/Knowledge	2.68	2.70	0.02	2.42	2.67	0.25	2.55	2.68	0.13
Encouraged to Use Analysis	5.00*	5.00*	0.00	4.72*	5.44*	0.72	4.86*	5.22*	0.36
Encouraged to Use Synthesis	2.68	2.57	-0.11	2.51	2.74	0.23	2.60	2.65	0.05
Can be Flexible	2.62	2.46	-0.16	2.58	2.75	0.17	2.60	2.60	0.00
Can Use Problem Solving	2.62	2.57	-0.05	2.56	2.86	0.30	2.59	2.71	0.12
Can Integrate Outside Info	5.19*	5.11*	-0.08	4.86*	5.44*	0.58	5.03*	5.27*	0.24
Can Use Analysis	2.53	2.47	-0.06	2.53	2.69	0.16	2.53	2.58	0.05
Can Use Synthesis	2.46	2.54	0.08	2.34	2.66	0.32	2.40	2.60	0.20

Note: * indicates a rating scale of 0-6 (6=higher ratings), all other ratings on a scale of 0-4 (4=higher ratings), bold indicates significant ($p \leq 0.05$) difference.

Table 6 Paired Samples Test for Heat Transfer Across Both Semesters

Pre to Post Variable	Differences				t	df	Sig. (2-tailed)
	Mean	Std. Dev.	95% Confidence Interval of the Difference				
			Lower	Upper			
Used Activities to Illustrate	-0.70	1.11	-0.99	-0.39	-4.69	55	0.000
Furthered Understanding	-0.40	1.20	-0.72	-0.08	-2.48	54	0.016
Encouraged to Use Analysis	-0.65	1.25	-1.00	-0.31	-3.77	51	0.000
Encouraged to Use Synthesis	-0.28	0.98	-0.55	-0.01	-2.08	53	0.042
Can be Flexible	-0.32	0.89	-0.55	-0.08	-2.68	56	0.010
Can Integrate Outside Info	-0.46	1.29	-0.81	-0.12	-2.69	55	0.010

Table 7 Paired Samples Test for Mass Transfer Across Both Semesters

Pre to Post Variable	Differences				t	df	Sig. (2-tailed)
	Mean	Std. Dev.	95% Confidence Interval of the Difference				
			Lower	Upper			
Used Activities to Illustrate	0.24	0.89	0.01	0.48	2.08	56	.042
Encouraged to Problem Solve	0.24	0.88	0.01	0.47	2.07	58	.042
Can Use Analysis	0.26	0.86	0.04	0.49	2.32	56	.024

Table 8 Paired Samples Test for Fluid Flow for Semester 3

Pre to Post Variable	Differences				t	df	Sig. (2-tailed)
	Mean	Std. Dev.	95% Confidence Interval of the Difference				
			Lower	Upper			
Easily Presented	0.74	1.05	0.42	1.07	4.65	42	.000
Furthered Understanding	0.47	1.03	0.15	0.78	2.96	42	.005

Table 9 Paired Samples Test for Fluid Flow for Semester 5

Pre to Post Variable	Differences				t	df	Sig. (2-tailed)
	Mean	Std. Dev.	95% Confidence Interval of the Difference				
			Lower	Upper			
Encouraged to Flexible	-0.31	0.80	-0.57	-0.05	-2.40	38	.021
Encouraged to Problem Solve	-0.31	0.80	-0.57	-0.05	-2.40	38	.021
Encouraged to Integrate Outside Materials/Knowledge	-0.31	0.66	-0.52	-0.10	-2.93	38	.006
Encouraged to Use Analysis	-0.90	1.07	-1.24	-0.55	-5.23	38	.000
Encouraged to Use Synthesis	-0.72	1.10	-1.07	-0.36	-4.08	38	.000
Can be Flexible	-0.33	0.77	-0.58	-0.08	-2.70	38	.010
Can Use Synthesis	-0.33	0.66	-0.55	-0.12	-3.14	38	.003

Table 10 Paired Samples Test for Reactor Design Across Semesters

Pre to Post Variable	Differences				t	df	Sig. (2-tailed)
	Mean	Std. Dev.	95% Confidence Interval of the Difference				
			Lower	Upper			
Encouraged to Flexible	-0.18	0.73	-0.35	-0.01	-2.08	72	.041
Encouraged to Problem Solve	-0.18	0.73	-0.35	-0.01	-2.08	72	.041
Encouraged to Integrate Outside Materials/Knowledge	-0.14	0.58	-0.27	-0.00	-2.00	72	.049
Encouraged to Use Analysis	-0.36	1.23	-0.64	-0.07	-2.48	72	.016
Can Use Synthesis	-0.19	0.74	-0.37	-0.02	-2.22	71	.030

Table 11 Paired Samples Test for Pre to Post Responses to Knowledge Questions in Reactor Design and Mass Transfer

Pre to Post Variable	Differences				t	df	Sig. (2-tailed)
	Mean	Std. Dev.	95% Confidence Interval of the Difference				
			Lower	Upper			
Reactor Design Single Questions	-1.29	0.97	-1.49	-1.09	-12.78	92	.000
Reactor Design Multiple Question	-1.41	0.90	-1.59	-1.22	-15.10	92	.000
Mass Transfer Single Questions	-1.33	0.89	-1.64	-1.03	-8.94	35	.000
Mass Transfer Multiple Question	-0.75	0.77	-1.01	-0.49	-5.84	35	.000